

Steady flow of one uniformly rotating fluid layer above another immiscible uniformly rotating fluid layer

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The steady laminar flow of two immiscible, uniformly rotating fluid layers is studied and exact similarity solutions of the axisymmetric Navier-Stokes equations in cylindrical polar coordinates are found. The similarity solutions occur with a flat interface at $z = 0$ under the parameter restriction that $\sigma^2 \rho = 1$, where σ is the ratio of the fluid angular velocities at $z = \pm\infty$ and ρ is the density ratio of the two fluids. Under this restriction the problem reduces to one with two independent parameters σ and μ , the viscosity ratio of the fluids. Numerical results of the resulting system of ordinary differential equations are found for selected values of μ and σ , and it is shown that similarity solutions exist for $\sigma_c(\mu) \leq \sigma \leq 1$, where $\sigma_c(\mu) < 0$ (i.e., counterrotating flows). For $\sigma < 0$ the lower fluid can become divided into two distinct recirculation regions between which fluid cannot transfer.

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I. INTRODUCTION

The investigation of rotating flows has a long history due to their significance in industrial applications, as well as being of fundamental interest. Such fluid flow systems can be wholly confined between two disks, or semiconfined, with the disk(s) rotating at a constant angular velocity and/or with the fluid in the far field undergoing constant rigid-body rotation. The study of these axisymmetric flows is motivated by their connection to both ocean circulation models and turbomachinery applications (see, e.g., [1] and references therein for a review). Further, investigation of these flows is also motivated by theoretical interest, e.g., determining exact solutions to the Navier-Stokes equations in particular geometries and setups.

The theoretical interest in these flows stems from the fact that for laminar flows, axisymmetric steady exact solutions to the Navier-Stokes equations can be found in the form of similarity solutions. These similarity solutions are of great interest because their existence allows for detailed theoretical studies of the flows, including determining the stability properties of such flows. However, the study of similarity solutions is only significant if they are physically realizable in experiments [2]. For laminar axisymmetric steady flows similar to those studied here, there is both numerical and experimental evidence which shows that similarity solutions act as an attractor for flows with weakly unsteady perturbations. For the flow produced by a steadily rotating infinite disk below a stationary fluid, the experiments of [3] confirmed the realization of the similarity solution of [4] to a high level of accuracy. The similarity solution of [5] generated by a rigidly rotating fluid above a fixed infinite disk is more difficult to realize experimentally due to the difficulty of producing a rigidly rotating infinite flow far from the disk. During their studies investigating flows with finite and infinite disks plus rigid rotation from the disk, Refs. [6,7] concluded that the Bödewadt solution

exists. Subsequently, by considering the spin-down of a cylindrical cavity, Refs. [8,9] showed that the Bödewadt solution is realizable locally at the end walls of the cylinder. This was later confirmed in the numerical calculations and experiments of [10,11], the latter study of which considered the spin-down of a cylindrical cavity in which only one end wall was impulsively stopped. It is claimed that this approach “may be as close as possible to . . . [Bödewadt flow] in a physically realizable finite domain.”

The flow examples documented above are ones consisting of only one type of fluid. For the case of flows consisting of two immiscible fluid layers, the literature is more limited, with only three problems known to have been investigated for the planar two-dimensional geometry, in which exact similarity solutions exist. The first [12] considered the velocity distribution between two parallel streams with the same configuration for the Kelvin-Helmholtz instability and calculated similarity solutions for a selection of parameters. The second study [13] considered a linear shear flow over a quiescent lower fluid far from the interface. The third, more recent work [14] studied the boundary layer that forms at the interface of two different linear shear flows and discovered an interesting feature of dual similarity solutions for some parameter range. However, only one branch of solutions turned out to be physically realizable.

In the present paper we analyze what may be considered the axisymmetric analog of Lock’s problem [12], namely, the flow generated by one viscous fluid layer (denoted by subscript 1) rotating at constant angular velocity ω_1 above a second immiscible viscous fluid layer (denoted by subscript 2) rotating at constant angular velocity ω_2 . This problem is three dimensional and it is found that exact similarity solutions exist in the restricted case $\rho\sigma^2 = 1$, where $\rho = \rho_2/\rho_1$ is the density ratio of the two fluids and $\sigma = \omega_2/\omega_1$. Here $\sigma > 0$ means the flows are corotating, while $\sigma < 0$ denotes counterrotating flows. We note at the outset that this problem was not considered in the book on two-fluid flows by Joseph and Renardy [15].

The presentation of the paper is as follows. The problem is formulated in Sec. II and numerical results for various values of $\mu = \mu_2/\mu_1$, the viscosity ratio of the two fluids, and σ are presented in Sec. III, along with velocity profiles in the radial, azimuthal, and axial directions. The paper concludes with a discussion in Sec. IV.

II. FORMULATION

Consider an incompressible upper fluid with velocity $\mathbf{u}_1 = (u_1, v_1, w_1)$, pressure p_1 , density ρ_1 , and viscosity μ_1 rotating at constant angular velocity ω_1 above an immiscible incompressible lower fluid with velocity $\mathbf{u}_2 = (u_2, v_2, w_2)$, pressure p_2 , density ρ_2 , and viscosity μ_2 rotating at constant angular velocity ω_2 . The velocity components are with respect to a cylindrical coordinate system (r, θ, z) and gravity is assumed to act parallel to the z axis. See Fig. 1 for a schematic of the system considered. Note that solutions are assumed to be steady and axisymmetric and that the interface is assumed to be flat, which means the effect of surface tension on the results can be neglected as there is zero interface curvature.

Nondimensionalizing lengths with $\sqrt{\nu_1/\omega_1}$, velocities with $\sqrt{\nu_1\omega_1}$, and pressure with $\rho_1\nu_1\omega_1$, where $\nu_1 = \mu_1/\rho_1$ is the kinematic viscosity in the upper layer, one arrives at the dimensionless Navier-Stokes equations in the upper layer as

$$(\mathbf{u}_1 \cdot \nabla)\mathbf{u}_1 = -\nabla(p_1 + F^{-1}\eta) + \nabla^2\mathbf{u}_1 \quad (\eta \geq 0), \quad (1a)$$

$$\nabla \cdot \mathbf{u}_1 = 0 \quad (1b)$$

and in the lower layer one finds

$$(\mathbf{u}_2 \cdot \nabla)\mathbf{u}_2 = -\frac{1}{\rho}\nabla(p_2 + \rho F^{-1}\eta) + \frac{\mu}{\rho}\nabla^2\mathbf{u}_2 \quad (\eta \leq 0), \quad (1c)$$

$$\nabla \cdot \mathbf{u}_2 = 0. \quad (1d)$$

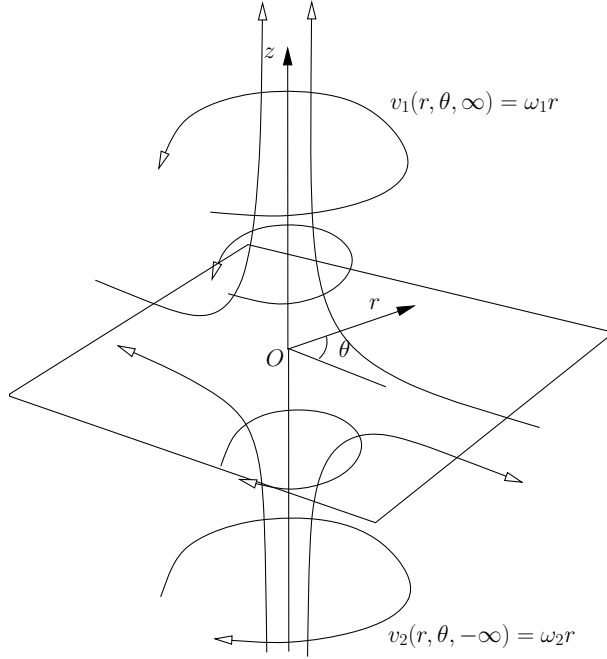


FIG. 1. Schematic diagram of the two-fluid rotating flow system considered. This figure depicts a counterrotating case.

Here the dimensionless axial variable is $\eta = z/\sqrt{v_1/\omega_1}$, $F = \omega_1\sqrt{v_1\omega_1}/g$ is the Froude number, and in (1c) the density and viscosity ratios are, respectively,

$$\rho = \frac{\rho_2}{\rho_1}, \quad \mu = \frac{\mu_2}{\mu_1}.$$

We posit the similarity form for the upper fluid layer satisfying continuity

$$u_1(r, \eta) = rf'_1(\eta), \quad v_1(r, \eta) = rg_1(\eta), \quad w_1(r, \eta) = -2f_1(\eta) \quad (2a)$$

and that for the lower fluid layer is

$$u_2(r, \eta) = rf'_2(\eta), \quad v_2(r, \eta) = rg_2(\eta), \quad w_2(r, \eta) = -2f_2(\eta). \quad (2b)$$

Application of far-field boundary conditions of constant rotation at ω_1 in the upper layer and constant rotation at ω_2 in the lower layer gives the far-field conditions in the upper layer

$$f'_1(\infty) = 0, \quad g_1(\infty) = 1 \quad (3a)$$

and in the lower layer

$$f'_2(-\infty) = 0, \quad g_2(-\infty) = \sigma, \quad (3b)$$

where the new dimensionless quantity is the ratio

$$\sigma = \frac{\omega_2}{\omega_1}.$$

Inserting the similarity forms (2) into the Navier-Stokes equations (1) leads to a pair of coupled ordinary differential equations (ODEs) in the upper layer

$$f_1''' + 2f_1f_1'' - f_1'^2 + g_1^2 - 1 = 0, \quad (4a)$$

$$g_1'' + 2(f_1g_1' - f_1'g_1) = 0, \quad (4b)$$

with the pressure field obtained from integrating the pair of equations (1a) as

$$p_1(r, \eta) = p_{10} + \frac{r^2}{2} - 2[f_1^2(\eta) + f_1'(\eta)] - F^{-1}\eta, \quad (4c)$$

where $p_{10} = p_1(0, 0)$ is a constant. In the lower layer the coupled ODE system is

$$\frac{\mu}{\rho} f_2''' + 2f_2 f_2'' - f_2'^2 + g_2^2 - \sigma^2 = 0, \quad (5a)$$

$$\frac{\mu}{\rho} g_2'' + 2(f_2 g_2' - f_2' g_2) = 0, \quad (5b)$$

with the pressure field obtained from integrating equations (1c) as

$$p_2(r, \eta) = p_{20} + \rho \left[\sigma^2 \frac{r^2}{2} - 2 \left(f_2^2(\eta) + \frac{\mu}{\rho} f_2'(\eta) \right) \right] - \rho F^{-1}\eta, \quad (5c)$$

where again $p_{20} = p_2(0, 0)$ is a constant.

The kinematic interfacial conditions stipulating continuity of the velocity field across the flat interface give

$$f_1(0) = f_2(0) = 0, \quad f_1'(0) = f_2'(0), \quad g_1(0) = g_2(0). \quad (6)$$

Then application of the interface stress jump conditions

$$[\tau_{zr}] = 0, \quad [\tau_{z\theta}] = 0, \quad [\tau_{zz}] = 0$$

give the results

$$g_1'(0) = \mu g_2'(0), \quad (7a)$$

$$f_1''(0) = \mu f_2''(0), \quad (7b)$$

and

$$p_2(r, 0) - p_1(r, 0) = 4[f_1'(0) - \mu f_2'(0)]. \quad (7c)$$

The systems of ODEs in each layer, (4) and (5), comprise two fifth-order systems, and hence require ten boundary and interfacial conditions for solution. In (3), (6), and (7) we have 11 conditions, so the system appears overspecified; however, inserting the expressions for the pressures from (4c) and (5c) into (7c) and applying $f_1(0) = f_2(0) = 0$ gives, after simplification, the result

$$p_{20} - p_{10} + \frac{r^2}{2}(\rho\sigma^2 - 1) + 2[\mu f_2'(0) - f_1'(0)] = 0. \quad (8)$$

We now apply $f_1'(0) = f_2'(0)$ from (6) and set coefficients of powers of r to zero to obtain

$$p_{20} - p_{10} = 2(1 - \mu)f_1'(0) \quad (9a)$$

and the critical relation

$$\rho\sigma^2 = 1, \quad (9b)$$

which is required for self-similarity. Thus (7c) is automatically satisfied if (9) holds and hence for this restriction of the parameter σ we have a well-defined problem.

Reiterating the coupled system of equations, for $\eta > 0$ we have

$$f_1''' + 2f_1 f_1'' - f_1'^2 + g_1^2 - 1 = 0, \quad (10a)$$

$$g_1'' + 2(f_1 g_1' - f_1' g_1) = 0, \quad (10b)$$

while for $\eta < 0$ we have

$$\mu\sigma^2 f_2''' + 2f_2 f_2'' - f_2'^2 + g_2^2 - \sigma^2 = 0, \quad (11a)$$

$$\mu\sigma^2 g_2'' + 2(f_2 g_2' - f_2' g_2) = 0, \quad (11b)$$

where $\rho = 1/\sigma^2$ has been eliminated. These are to be solved with far-field conditions

$$f_1'(\infty) = 0, \quad g_1(\infty) = 1, \quad (12a)$$

$$f_2'(-\infty) = 0, \quad g_2(-\infty) = \sigma, \quad (12b)$$

along with the interfacial conditions

$$f_1(0) = f_2(0) = 0, \quad f_1'(0) = f_2'(0), \quad g_1(0) = g_2(0), \quad (13a)$$

$$\mu f_2''(0) = f_1''(0), \quad \mu g_2'(0) = g_1'(0). \quad (13b)$$

Thus the steady solution of two fluids in solid-body rotation is governed by two parameters: $\mu > 0$ and σ . For stability without rotation in either layer in the presence of gravity, we take $\rho \geq 1$, which restricts the angular velocity ratio to $0 \leq \sigma^2 \leq 1$. Note that the lower layer can counterrotate relative to the upper layer. The case when $\sigma = 0$ (or $\rho = \infty$) corresponds to replacing the lower fluid with a solid wall at $\eta = 0$. Hence, in the limit $\sigma \rightarrow 0$ we expect flow variables, such as the shear stresses at $\eta = 0$, to tend to those of the Bödewadt problem [5].

III. RESULTS

In this section we present numerical solutions of the system of equations (10) and (11) with far-field and interfacial conditions (12) and (13), respectively, for various values of μ and σ . To aid the numerical computations for small values of $\mu\sigma^2$, where the lower layer ODEs become singular, we introduce the change of variables in layer 2, viz.,

$$\zeta = -\mu^{-1/2}\sigma^{-1}\eta, \quad F_2(\zeta) = \mu^{-1/2}\sigma^{-1}f_2(\eta), \quad G_2(\zeta) = g_2(\eta),$$

which removes the singular term from the highest derivative and changes the integration range to $\zeta \in [0, \infty]$ (the same as the η domain), which means that both sets of equations can now be solved simultaneously on the same interval. The equations are solved by numerically integrating from the interface at $\eta = 0$ out to $\eta = \eta_{\max}$ and the four interfacial unknowns $f_1'(0)$, $f_1''(0)$, $g_1(0)$, and $g_1'(0)$ are updated via Newton iterations using the far-field conditions (12). For the results presented we integrated out to $\eta_{\max} = 20$ with a step size $\Delta\eta = 10^{-4}$ in order to obtain converged grid-independent results.

For small and negative values of σ , integrating to $\eta_{\max} = 20$ becomes more troublesome as the solutions are more sensitive to the accuracy of the interface unknowns. This can cause the shooting approach to fail. To overcome this we use the shooting-splitting method of [16] which splits the integral domain into N subdomains. In each subdomain the unknown variables at the smaller η end of the subdomain are integrated to the junction with the next subdomain and then these unknowns are updated, via Newton iterations, using the continuity of the solution and its derivatives across subintervals. This process continues until the results converge. This approach leads to a larger set of nonlinear equations to solve than the simple shooting approach ($10N \times 10N$ in this case), but the exponential growth of the solution is now restricted in each subdomain and hence there is higher chance of convergence. We find that $10 \leq N \leq 20$ for this problem is sufficient to gain the converged solutions presented below.

A. Positive σ results

We have chosen viscosity ratios $\mu = \{0.1, 0.2, 0.5, 1.0, 2.0, 5.0, 10.0\}$ to present the overall behavior of the flow. First we display the upper layer radial stress parameter $f_1''(0)$ as a function of σ in Fig. 2 and the variation of the upper layer azimuthal stress parameter $g_1'(0)$ is shown in

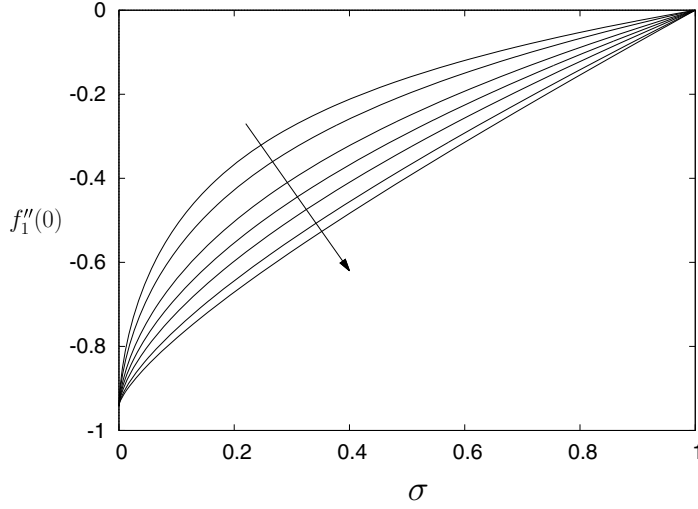


FIG. 2. Variation of upper interfacial radial stress parameter $f_1''(0)$ with positive values of σ at $\mu = \{0.1, 0.2, 0.5, 1.0, 2.0, 5.0, 10.0\}$ with the arrow in the direction of increasing values of μ .

Fig. 3. These show that as the viscosity of the lower layer is increased (μ increasing) both the radial and azimuthal stresses at the interface increase in magnitude for fixed σ . As $\sigma \rightarrow 0$ we observe that all the results agree with the [5] result

$$f_1'(0) = g_1(0) = 0, \quad f_1''(0) = -0.941\,97, \quad g_1'(0) = 0.772\,89.$$

The radial and azimuthal interfacial velocities $f_1'(0)$ and $g_1(0)$, on the other hand, decrease in absolute magnitude at a fixed σ for increasing μ , as seen in Figs. 4 and 5, respectively. The radial interfacial velocity is always directed towards the origin [$f_1'(0) < 0$] for all values of $0 \leq \sigma \leq 1$ and reaches a maximum absolute magnitude somewhere in $0 \leq \sigma \lesssim 0.2$. However, the value of $f_1'(0)$ for $\sigma > 0$ is an order of magnitude smaller than the azimuthal interface velocity $g_1(0)$.

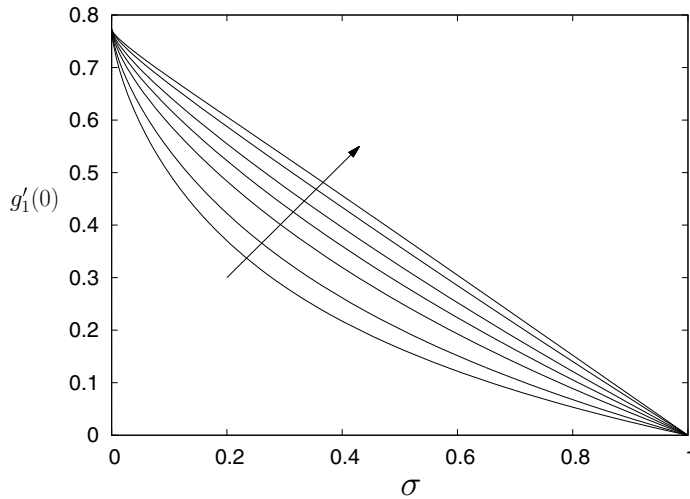


FIG. 3. Variation of upper interfacial azimuthal stress parameter $g_1'(0)$ with positive values of σ at $\mu = \{0.1, 0.2, 0.5, 1.0, 2.0, 5.0, 10.0\}$ with the arrow in the direction of increasing values of μ .

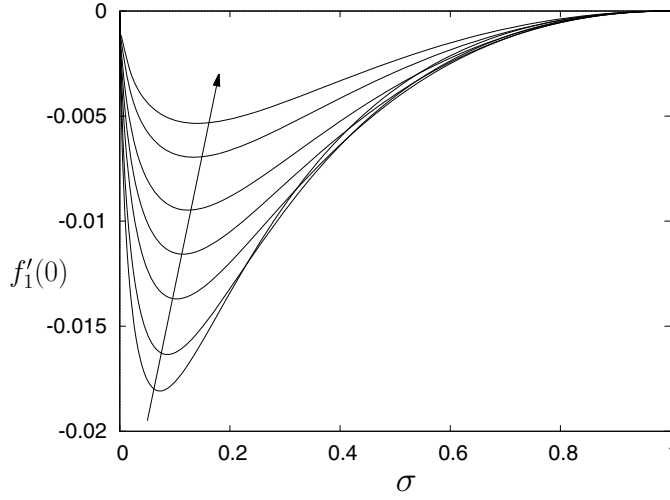


FIG. 4. Upper layer interfacial radial velocity $f'_1(0)$ for positive values of σ at $\mu = \{0.1, 0.2, 0.5, 1.0, 2.0, 5.0, 10.0\}$ with the arrow in the direction of increasing values of μ .

In Figs. 6 and 7 we present the upper layer far-field axial velocity parameter $f_1(\infty)$ and the lower layer far-field axial velocity parameter $f_2(-\infty)$, respectively. These show that in the upper layer the fluid in the far field is directed away from the interface ($w_1 > 0$), while in the lower layer the fluid is directed towards the interface ($w_2 > 0$). Therefore, to conserve mass, the upper layer must have a net inflow of fluid spiraling in from $r = \infty$ close to $\eta = 0$, while for the lower layer there must be a corresponding net outflow spiraling out towards $r = \infty$. This inflow-outflow behavior either side of $\eta = 0$ creates a strong shear layer across this interface as seen in Sec. III C. Note that in an oceanographical context, the upper layer motion is synonymous with Ekman pumping, with fluid pumped in along the interface and out to $\eta = \infty$, while in the lower layer motion is

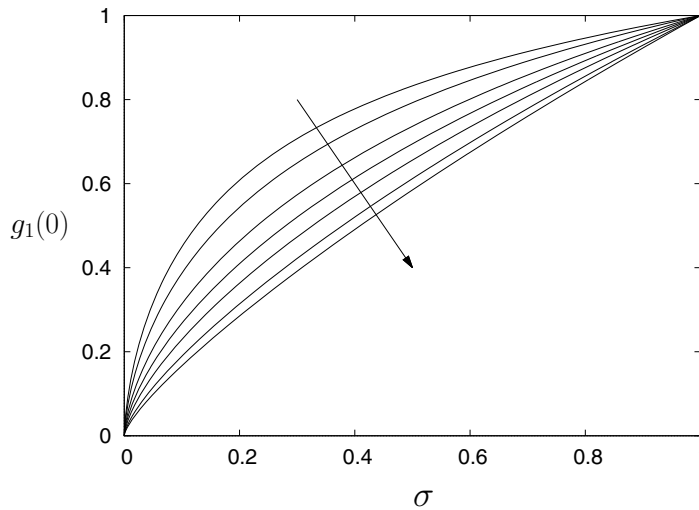


FIG. 5. Upper layer interfacial azimuthal velocity $g_1(0)$ for positive values of σ at $\mu = \{0.1, 0.2, 0.5, 1.0, 2.0, 5.0, 10.0\}$ with the arrow in the direction of increasing values of μ .

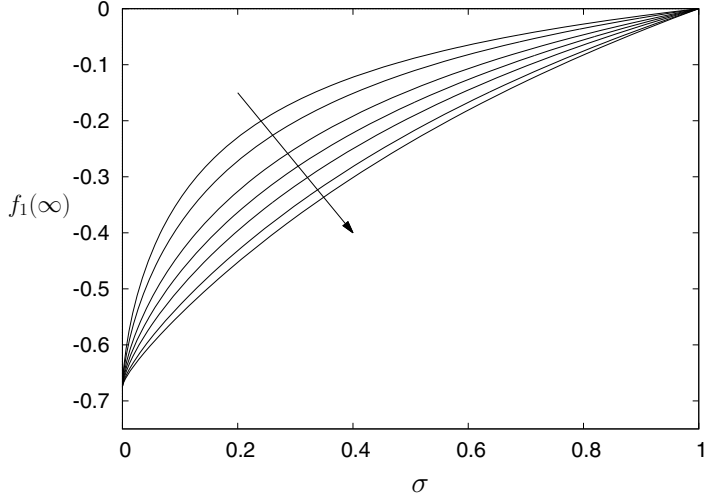


FIG. 6. Variation of far-field behavior of the axial velocity parameter in the upper layer $f_1(\infty)$ with positive values of σ at $\mu = \{0.1, 0.2, 0.5, 1.0, 2.0, 5.0, 10.0\}$ with the arrow in the direction of increasing values of μ .

synonymous with Ekman suction, with fluid sucked up from $\eta = -\infty$ and out along the interface [17]. Comparing this result to two of the most common rotating flow solutions, the von Kármán flow has an inflow of fluid from $\eta = \infty$ while the Bödewadt flow has an outflow of fluid at $\eta = \infty$. Hence there appear to be similarities of the upper layer flow and the Bödewadt result, and the lower layer flow and the von Kármán result. This is further explored in Sec. III C.

B. Negative σ results

Here again we present results for the same viscosity ratios as in Sec. III A. The upper layer radial stress parameter $f_1''(0)$ is plotted in Fig. 8 as a function of σ , while the upper layer azimuthal stress

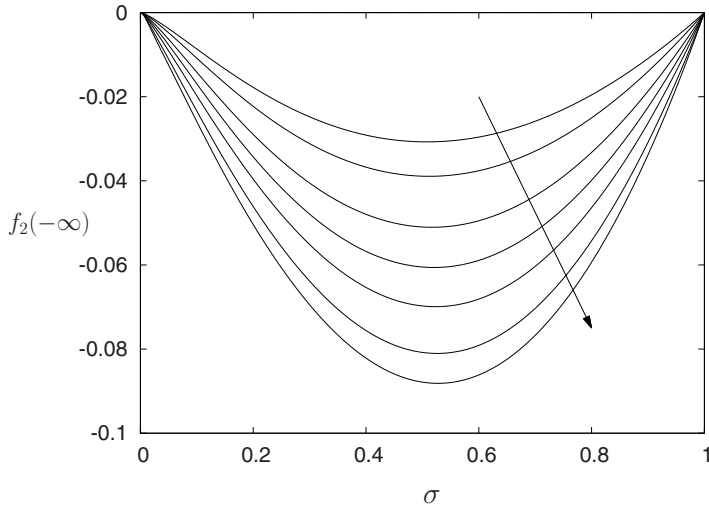


FIG. 7. Variation of far-field behavior of axial velocity parameter in the lower layer $f_2(-\infty)$ with positive values of σ at $\mu = \{0.1, 0.2, 0.5, 1.0, 2.0, 5.0, 10.0\}$ with the arrow in the direction of increasing values of μ .

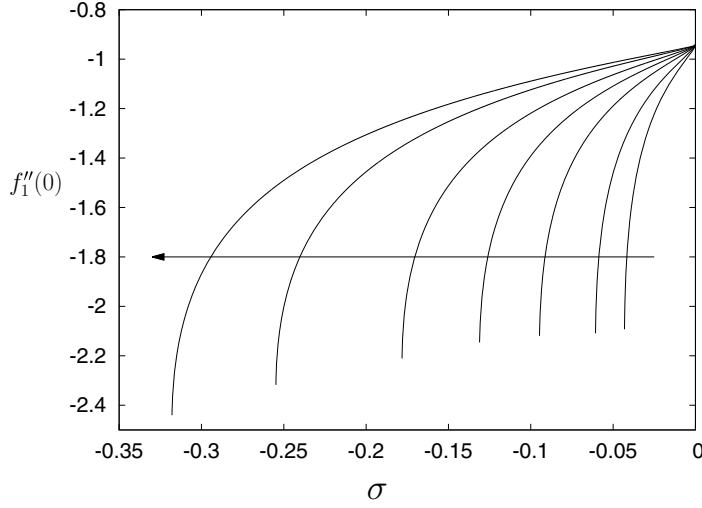


FIG. 8. Variation of upper interfacial radial stress parameter $f_1''(0)$ with negative values of σ at $\mu = \{0.1, 0.2, 0.5, 1.0, 2.0, 5.0, 10.0\}$ with the arrow in the direction of increasing values of μ .

parameter $g_1'(0)$ is plotted in Fig. 9. Here, for each value of μ , the absolute magnitudes of $f_1''(0)$ and $g_1'(0)$ increase with decreasing σ , down to some critical value $\sigma = \sigma_c$, where the numerical scheme fails to converge. For $\sigma < \sigma_c$ there are no similarity solutions of the form (2). The radial and azimuthal interfacial velocities are given in Figs. 10 and 11, respectively, and both increase in absolute magnitude down to $\sigma = \sigma_c$. Here we observe that $g_1(0)$ has now switched sign from the $\sigma > 0$ case in Sec. III A while all other interfacial parameters retain the same sign.

The upper layer far-field axial velocity parameter $f_1(\infty)$ and the lower layer far-field axial velocity parameter $f_2(-\infty)$ are presented in Figs. 12 and 13, respectively. As in Sec. III A for $\sigma > 0$, the upper layer far-field flow remains directed away from the interface. The absolute magnitude of

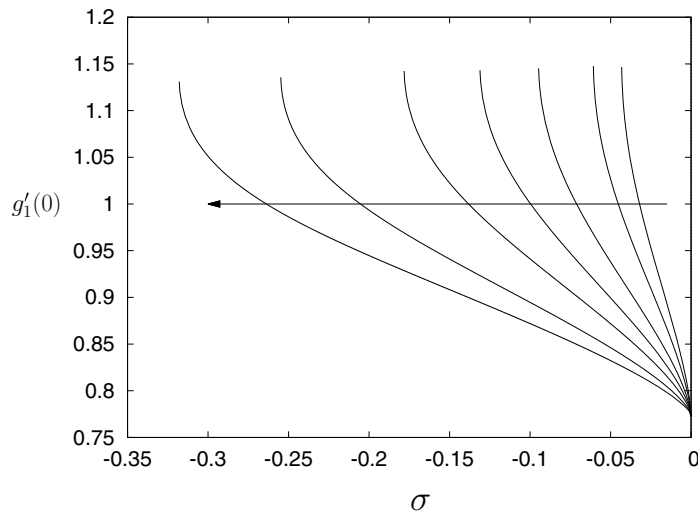


FIG. 9. Variation of upper interfacial azimuthal stress parameter $g_1'(0)$ with negative values of σ at $\mu = \{0.1, 0.2, 0.5, 1.0, 2.0, 5.0, 10.0\}$ with the arrow in the direction of increasing values of μ .

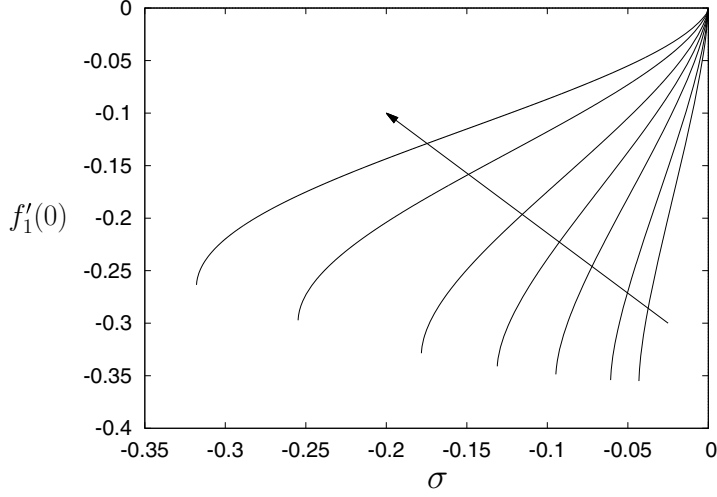


FIG. 10. Upper layer interfacial radial velocity $f'_1(0)$ for negative values of σ at $\mu = \{0.1, 0.2, 0.5, 1.0, 2.0, 5.0, 10.0\}$ with the arrow in the direction of increasing values of μ .

this outflow increases initially as σ reduces from zero to attain a maximum magnitude [minimum of $f_1(\infty)$] before decreasing in absolute magnitude as $\sigma \rightarrow \sigma_c$. In the lower layer, on the other hand, an outflow ($w_2 < 0$) is observed for small $|\sigma|$ at all values of μ . In the results presented, for $\mu \leq 2$ this outflow switches back to an inflow as $\sigma \rightarrow \sigma_c$, while for $\mu = 10$ the flow remains an outflow as $\sigma \rightarrow \sigma_c$. For intermediate cases, such as $\mu = 5$, the axial flow at $\eta = -\infty$ can alternate between an outflow to an inflow and back to an outflow as σ decreases from zero. Finally, the variation of the limiting negative values σ_c plotted as a function of μ in Fig. 14 shows that this value decreases as μ increases.

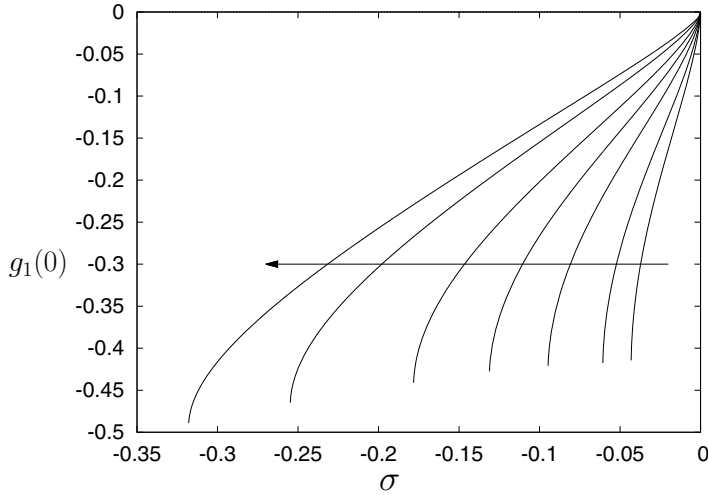


FIG. 11. Upper layer interfacial azimuthal velocity $g_1(0)$ for negative values of σ at $\mu = \{0.1, 0.2, 0.5, 1.0, 2.0, 5.0, 10.0\}$ with the arrow in the direction of increasing values of μ .

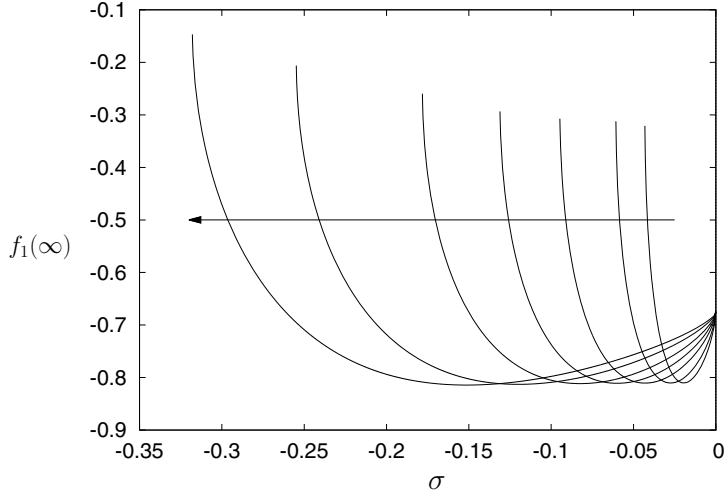


FIG. 12. Variation of far-field behavior of the axial velocity parameter in the upper layer $f_1(\infty)$ with negative values of σ at $\mu = \{0.1, 0.2, 0.5, 1.0, 2.0, 5.0, 10.0\}$ with the arrow in the direction of increasing values of μ .

C. Velocity profiles

Here we present the radial and azimuthal velocity profiles for $\mu = 1$ at $\sigma = \{-0.1, 0.0, 0.2, 0.5, 0.8\}$. In all cases we plot both upper and lower layer results together to show the transition across the $\eta = 0$ interface. The radial velocity profiles plotted in Fig. 15 show that the radially inward wall jet above the interface increases significantly as σ is reduced to $\sigma = -0.1$, and there is a weak radially outward wall jet just below the interface for all values of σ . In Fig. 16 the azimuthal profiles exhibit an overshoot in the upper layer close to the interface whose magnitude increases with decreasing σ . Note that all velocities are positive for $\sigma > 0$ but that for $\sigma = -0.1$ there is the expected counterrotation exhibited in the lower layer. These overshoots in the azimuthal velocity

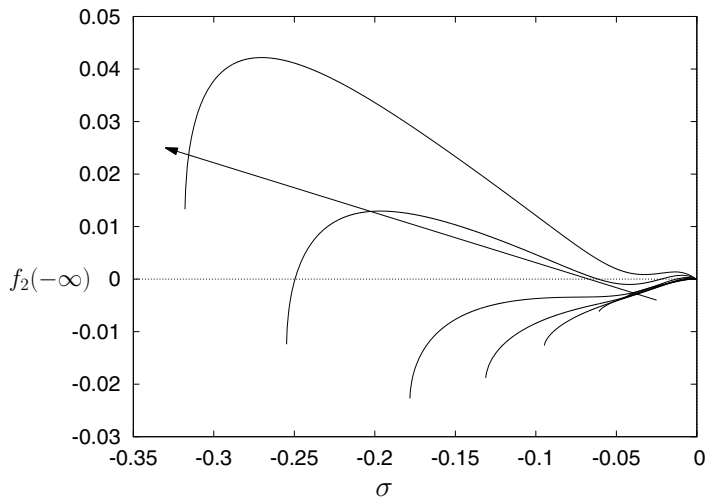
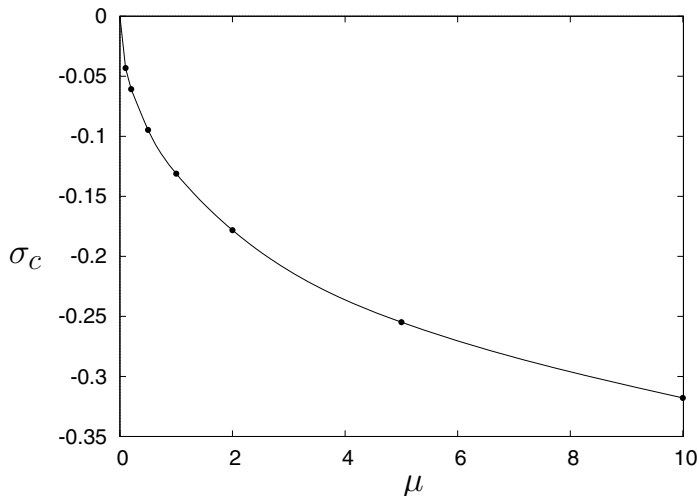


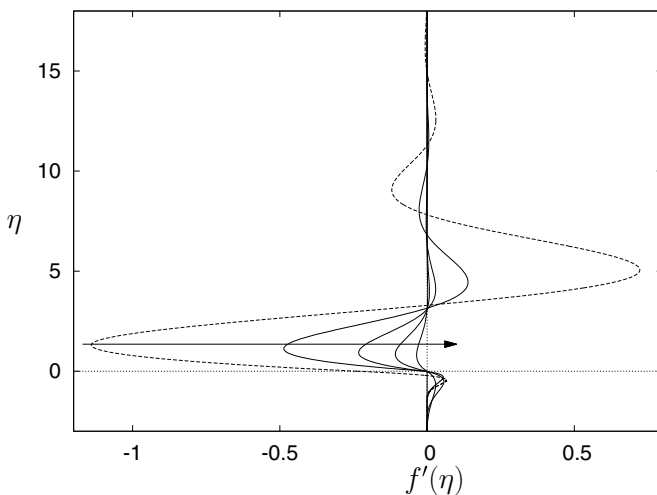
FIG. 13. Variation of far-field behavior of axial velocity parameter in the lower layer $f_2(-\infty)$ with negative values of σ at $\mu = \{0.1, 0.2, 0.5, 1.0, 2.0, 5.0, 10.0\}$ with the arrow in the direction of increasing values of μ .


 FIG. 14. Variation of the limiting values σ_c for negative values of σ as a function of μ .

profile lead to a large shear flow across the interface which ultimately leads to the breakdown of the similarity solution.

As mentioned at the end of Sec. III A, there are distinct similarities between the upper layer flow and the Bödewadt flow and similarities between the lower layer flow and the von Kármán flow. These similarities are also evident in Figs. 15 and 16. Both the radial and azimuthal velocity profiles in the upper layer oscillate about their $\eta \rightarrow \infty$ value, for all σ values, in the same way that the Bödewadt solution does (see [18] for velocity profiles). In the lower layer the radial velocity increases to a maximum value before decaying exponentially to zero, while the azimuthal component decays exponentially (with a small amount of overshoot) to its far-field value, akin to the profiles for the von Kármán flow (see [19] for velocity profiles).

Finally, in Fig. 17 we plot profiles for the axial velocity $w = -2f(\eta)$. One observes that this velocity is positive in both the upper and lower layers except for $\sigma = -0.1$, which has an overshoot


 FIG. 15. Plot of both upper and lower layer radial velocity profiles $f'(\eta)$ for $\mu = 1$ at $\sigma = \{-0.1, 0.0, 0.2, 0.5, 0.8\}$ with the $\sigma = -0.1$ profile plotted as the dashed line. The arrow denotes the direction of increasing σ .

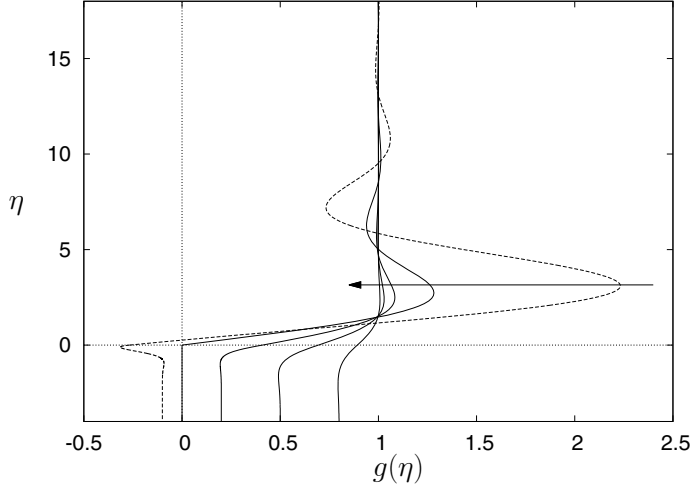


FIG. 16. Plot of both upper and lower layer azimuthal velocity profiles $g(\eta)$ for $\mu = 1$ at $\sigma = \{-0.1, 0.0, 0.2, 0.5, 0.8\}$ with the $\sigma = -0.1$ profile plotted as the dashed line. The arrow denotes the direction of increasing σ .

to negative values near the interface. This region of negative axial flow below the interface signifies a separate region of recirculating flow in which the fluid cannot escape to $\eta = -\infty$ [due to $-2f_2(\eta) = 0$ at $\eta = -0.67$]. This isolated layer of fluid motion is in contrast to the $\sigma > 0$ case where $-2f_1(\eta) = 0$ only at $\eta = 0$.

IV. DISCUSSION AND CONCLUSION

We have investigated the steady laminar flow generated by one incompressible fluid layer rotating with constant angular velocity ω_1 above a second immiscible, incompressible fluid layer rotating

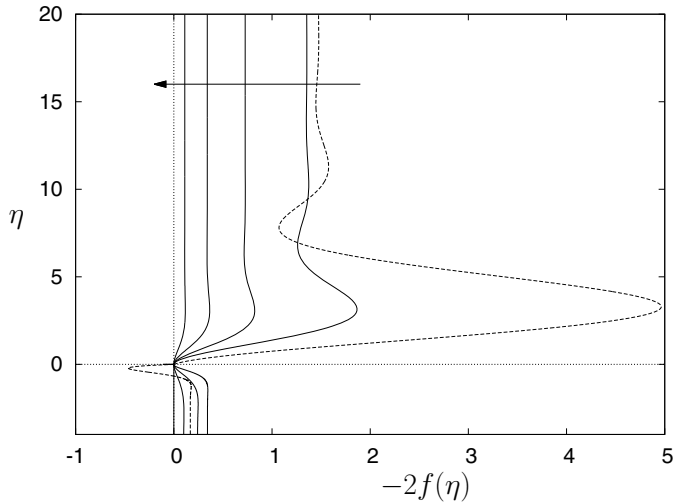


FIG. 17. Plot of both upper and lower layer axial velocity profiles $-2f(\eta)$ for $\mu = 1$ at $\sigma = \{-0.1, 0.0, 0.2, 0.5, 0.8\}$ with the $\sigma = -0.1$ profile plotted as the dashed line. The arrow denotes the direction of increasing σ .

with constant angular velocity ω_2 . By seeking exact solutions to the axisymmetric Navier-Stokes equations in the form of similarity solutions, we find that the problem can be formulated as four coupled ODEs, dependent upon two parameters $\mu = \mu_2/\mu_1$ and $\sigma = \omega_2/\omega_1$, where μ_i for $i = 1, 2$ is the dynamic viscosity in each layer. Matching the velocities and stresses of the flows across the interface at $\eta = 0$, we find similarity solutions under the restriction $\sigma^2\rho = 1$, where $\rho = \rho_2/\rho_1$ is the density ratio and $-1 \leq \sigma \leq 1$ for static stability under the influence of gravity.

Numerical results show that the similarity solutions exist for $\sigma_c(\mu) \leq \sigma \leq 1$, where $\sigma_c(\mu) < 0$, i.e., for all corotating flows similarity solutions exist, but only weak counterrotation can support such a solution. Also, for corotating flows the far-field axial velocities are always transported in the same direction (away from the interface as $\eta \rightarrow \infty$ and toward the interface as $\eta \rightarrow -\infty$), while for counterrotating flows both these axial flows can transport away from the interface depending on the value of σ . Another interesting feature for counterrotating flows is that an additional layer of recirculating fluid motion can form below the interface (i.e., $w_2 = 0$ at $\eta = 0$ and $\eta = -\eta_0$), in contrast to corotating flows where the axial velocity is only zero at $\eta = 0$. This behavior for $\sigma < 0$ is dependent on μ .

An interesting comparison is made here for fluid uniformly rotating at angular velocity ω above an infinite disk rotating at angular velocity Ω for which we define $\sigma = \omega\Omega$. Rogers and Lance [20] studied the problem of corotation and found solutions over the entire range $0 \leq \sigma < \infty$; thus, in the range $0 \leq \sigma \leq 1$ solutions are found for both the fluid-disk problem and the fluid-fluid problem. For counterrotating flow, Rogers and Lance found solutions down to $\sigma = -0.15$ but after that encountered difficulties. This was further studied by Weidman and Redekopp [21], who found that a singularity appears at $\sigma \simeq -0.154$; thus, like the fluid-fluid problem, the fluid-disk problem has only a small range of negative values of σ for which solutions are possible.

It is noted that the same limited range of similarity solutions has also been observed in the Falkner-Skan boundary layer flow [22]. This breakdown of the similarity solution for $\sigma < \sigma_c$ is interesting and warrants further study. The failure is likely due to the radial structure breaking down due to the large shear at the interface creating steady regions of recirculation and hence nonsimilarity or because no solutions with a flat interface [$\eta = h(r, \theta) = 0$] exist, in which case the shape of the interface also needs to be determined as part of the solution. It could also be possible that no steady solutions exist.

Throughout this paper the focus has been on calculating the existence of exact, steady, laminar similarity solutions to the Navier-Stokes equations. These steady solutions act as an attractor for unsteady solutions and the existence of these laminar solutions in practical experiments depends on the stability properties of the flow. As we observed, the velocity profiles have a curious form, combining features of both the von Kármán and Bödewadt flows below and above the interface respectively. From this observation alone we would expect this flow to have stability properties related to these two flows, i.e., we would expect them to contain both convective and absolute instability features which have been widely documented in the literature on these flows (see [8–10, 23–26] and references therein). In the stability calculation scenario, waves are assumed to have formed on the fluid interface; thus flow features such as surface tension become significant in determining whether the laminar flow is physically realizable or whether the flow breaks up into turbulence. The study of the linear stability of these flows is left as future work so as not to detract attention from the significant exact solutions to the axisymmetric Navier-Stokes equations presented here.

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